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### INTERMOUNTAIN POWER SERVICE CORPORATION

APR - 9 2001

LLG&M

27300 37300 00427

April 4, 2001

Richard Sprott, Director Division of Air Quality Department of Environmental Quality P.O. Box 144820 Salt Lake City, UT 84114-4820

Dear Director Sprott,

#### NOTICE OF INTENT: Modification of Source

Intermountain Power Service Corporation (IPSC) is hereby submitting a Notice of Intent (NOI) to increase generating capacity at the Intermountain Generating Station (IGS) in Delta. The IGS is a coal fired steam-electric plant located in Millard County, a NAAQS Attainment Area. Specifically, IPSC intends to construct modifications to Units One and Two at IGS to enhance performance and reliability and to allow increased capacity by de-bottlenecking certain aspects of our operation. This NOI requests an approval order to construct and a revision to IPSC's Title V permit to incorporate these modifications.

As required by UAC R307-401-2, the following information is provided:

(1) PROCESS DESCRIPTION: IGS is a fossil-fuel fired steamelectric generating station that primarily uses coal as fuel for the production of steam to generate electricity (SIC Code 4911). Both bituminous and subbituminous coals are utilized. Fuel oil and used oil are also combusted for light off and energy recovery.

IGS is a two unit facility operating at a rated capacity of 875 megawatts (MW) per unit (gross). Approximately 5.3 million tons of coal and 600,000 gallons of oil (including used oil) are used each year in the production of electricity. Boiler capacity is rated at 6.2 million pounds per hour of steam flow at 2822 psi.

IGS has in place bulk handling equipment for the unloading, transfer, storage, preparation, and delivery of solid and liquid fuel to the boilers. No changes of this equipment are proposed. No changes in the usage of other raw materials or bulk chemicals are planned.

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PROPOSED CHANGES: IPSC is planning to enhance steam flow characteristics through the high pressure (HP) section of each turbine used to generate electricity. This involves the replacement of the HP section with a modified design that improves performance and reliability. This modification in and of itself will not increase plant capacity, but will instead lower emissions due to decreased fuel use from the resulting increased performance.

Combined improvements to other areas of the plant will increase plant generating capacity. These modifications consist of "de-bottlenecking" critical points that presently prevent the full utilization of present equipment. Other changes are needed for reliability, performance and/or routine maintenance purposes. See Item 8 for details.

- characteristics of the emissions are expected to change as a result of the proposed modifications as indicated in the attached spreadsheet (Attachment 1), which shows the anticipated changes in emission rates, temperature, air contaminant types, and concentration of air contaminants. The mass flow of chimney effluent may change proportionately with the fuel usage and combustion at a heat input comparable to the current heat input. The existing pollution control devices include low-NOx burners, fabric filters and wet scrubbers.
  - (3) POLLUTION CONTROL DEVICE DESCRIPTION: The existing pollution control device equipment includes dual register low NOx burners, baghouse type fabric filters for particulate removal, and flue gas desulfurization scrubbers. The existing low NOx burners provide a nominal 60% reduction in potential combustion NOx formation, the baghouse filters operate at nominal 99.95% efficiency, and the wet scrubbers operate at nominal 90% efficiency. Control equipment for the handling and transfer of solid material include dust collection filters.

The project includes modifications to the flue gas flow through scrubber modules to enhance  $SO_2$  and acid gas removal rates. Also, the project includes installation of moderately improved NOx controls, such as the replacement of the existing dual register low NOx burners with new technology staged combustion low NOx burners.

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- (4) EMISSION POINT: The present emission point for the IGS boilers is a lined chimney that discharges at 712 feet above ground level (5386 feet above sea level). The chimney location is 39° 39' 39" longitude, 112° 34' 46" latitude (UTM 4374448 meters Northing, 364239 meters Easting.).
- (5) SAMPLING/MONITORING: Emissions from boiler combustion are continuously sampled and monitored at the chimney for nitrogen oxides, sulfur oxides, carbon dioxide, and volumetric flow. Opacity is measured at the fabric filter outlet. Other parameters recorded include heat input and production level (megawatt load). Monitoring will remain unchanged. Other emissions not directly monitored are calculated using engineering judgement, emission factors, and fuel analyses. The type and location of the monitors will not be changed.
- (6) OPERATING SCHEDULE: IGS operates 24 hours per day, seven days per week. This will not change as a result of the proposed modifications.
- (7) CONSTRUCTION SCHEDULE: Construction of the modifications will be performed in a staged manner, generally following the attached schedule. (See Attachment 2.)
- (8) MODIFICATION SPECIFICATIONS: The changes covered by this NOI include:
  - High Pressure Turbine Retrofit:

The high pressure turbine on each unit at IGS is scheduled to be replaced with a current technology, high efficiency turbine. This unit will increase high pressure turbine efficiency from approximately 84% to over 92%. Additionally, the turbine will be sized to provide up to 8.6% additional output.

### • Cooling Tower Performance Upgrade:

The cooling towers on each unit at IGS are scheduled for performance enhancement modifications to increase heat rejection capacity. Also, cooling tower transformers feeding the cooling tower fan motors will be upgraded. A study will be performed to identify and resolve needed redundancy issues for operation at new output levels.

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#### Boiler Safety Valve Additions:

Currently, a review is underway focusing on existing boiler safety valve capacity. Addition of one main steam safety valve on each unit is expected in order to address reliability concerns with the existing valves and to accommodate planned increase in generation capacity.

#### • Generator Cooling Enhancement:

An engineering evaluation is currently underway to identify any enhancements required on the generator in order to accommodate the planned 8.6% increase in generator output. The anticipated result of this evaluation is an upgrade to the current generator and stator cooling systems.

#### Isophase Bus Cooling Enhancement:

An engineering evaluation is currently underway to identify any enhancements required on the 26kv generator electrical bus feeding the main step-up transformer. The anticipated result of this evaluation is an upgrade to the current isophase bus duct cooling systems.

#### • Large Motor Bus Loading Equalization:

An engineering evaluation is currently underway to equalize the loading between the large and small motor bus. Due to limited tap adjustment capability on the auxiliary transformers feeding these load centers, several motors must be moved from one supply to the other in order to maintain required motor terminal voltages as unit output is increased.

#### Boiler Feed Pump Performance Upgrade:

The boiler feed pump manufacturer has notified IPSC of several enhancements they now offer that address previous reliability concerns and allow for small increases in output. These include, improved bearing housings, flow path smoothing, and impeller clearance modifications. These modifications provide for increased pump output at acceptable reliability levels.

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## Main Step-up Transformer Cooling:

The step-up transformer cores currently run close to their nominal temperature ratings when ambient temperatures are high. Proposed modifications are directed at increasing the cooling system capacity for cooling the transformer oil, core, and housing.

## NOx Reduction Project:

Some moderate NOx control systems will be added or enhanced. Recent advances in the burner industry have resulted in published operational data with improved NOx removal efficiencies. Within this project, burners in Unit 1 may be replaced with latest technology LNBs. Following successful testing, Unit 2 burner replacements would follow in successive outage upgrades. Alternatively, we may look at other technologies, or a combination of commercially available control systems. The installation of moderate NOx controls is expected to prevent any significant net increases of NOx due to increased capacity.

## • Scrubber Wall Ring:

Scrubber wall ring technology has been developed and patented in recent years to address inefficient flow patterns that routinely develop within the absorber vessels. This ring would be installed within all twelve (12) scrubber absorber vessels to move flow back to the center of the vessel, providing more efficient  $SO_2$  and acid gas scrubbing of the flue gas.

# • Generator Stator Cooling Water Oxygen Monitoring System:

Given concerns in recent years regarding the long term integrity of the generator stator bars, an oxygen monitoring system, capable of early identification of stator bar degradation is essential. As load increases, stator bar temperature and cooling flow velocities are also expected to rise. This system will guard against unexpected degradation of the stator.

• High Pressure Heater Drain Line Modifications:
An existing resonant vibration occurring in the high pressure heater drain line to the deaerator has become an increasing concern. The vibration appears to increase with load. An increase in unit output would require a modification to eliminate this concern.

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#### Boiler Modifications:

A comprehensive study is currently underway with the manufacturer of the boilers (Babcock & Wilcox). This study has been designed to review all aspects of boiler operation at the new turbine output levels. This study includes evaluation of current technologies and operating practices for minimizing emissions. The study will provide recommendations for modifying the existing boilers for stable and efficient operation at the new higher rating.

## Circulating Water Makeup Modifications:

Current circulating water makeup capacity is inadequate for increased unit production. A new design will support increased makeup requirements and return a degree of redundancy to the system, as originally designed.

## Boiler and turbine control system logic software & controls:

Upgrade of the existing control system includes complete replacement of the plant information system, control system simulator, coordinated control system, turbine control systems, combustion control systems and the alarm indication system. The new control systems will eliminate parts availability and reliability issues as well as providing the increased control system capacity required for the projects associated with the increased unit output. Boiler and turbine operating parameters are controlled within closer tolerances, resulting in less upsets and better emission control.

The capital expenditures for these changes to both units is expected to be about \$35 million. More detailed engineering specifications and project descriptions can be provided as needed.

PRODUCTION SUMMARY: The proposed project will increase generation capacity from 875 to approximately 950 MWhe, with steam flow design increasing from 6.2 to 6.9 million pounds per hour. Design heat input will increase from 8,352 to 9,225 million BTU per hour, requiring an increase from 5.3 to 5.6 million tons of coal each year. See Attachment 1 for details.

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> ADDITIONAL INFORMATION: IGS operates under a Title V permit (#2700010001). IPSC intends to continue to operate in full compliance with that permit and applicable requirements. No deviations from permit conditions are expected. IPSC requests that this NOI also be considered a request for revision of the Title V permit, and requests that the conditions of the approval order be incorporated into the Title V permit once the approval order is issued.

Operating Flexibility

IPSC reserves the right to cancel any and all planned modifications at any time. IPSC may only install the turbine dense packs, which by themselves would not require review as a major modification. We note that EPA has previously determined that enhancements like the Dense Pack project are not major modifications if there is no significant net increase in emissions. (See letter from Francis X. Lyons, Regional Administrator, EPA Region 5 to Henry Nickel of Hunton & Williams, dated 5/23/00.) If IPSC decides to install only the Dense Pack enhancements and certain upgrades for reliability, IPSC will provide the supporting information to show that there will be no significant net increase in emissions.

#### Phased Permitting

Due to the length and intermittent nature of the construction schedule for the proposed modifications, IPSC requests that the approval order contain terms that take into account the phases of installation. For example, due to lead times for engineering and budgeting, some portions of the project which affect capacity and/or emissions may be installed prior to upgrades in pollution IPSC would be receptive to an approval order control equipment. that includes interim emission limits for the period prior to project completion and final upgrades to control equipment.

Permit "Off Ramps"

Budgeting for the proposed project will be considered on a fiscal year-by-year basis. Although the current business climate for increased capacity is very favorable for this project, outlooks may change. Accordingly, IPSC proposes that the approval order contain conditions which provide that pollution control upgrades will be required only if those "debottlenecking" projects go forward which, if installed without controls, would increase the potential to emit enough to require major modification review. If IPSC decides not to complete certain portions of this project, the approval order should be structured so that IPSC is not forced to proceed with project completion.

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## NSPS/PSD Applicability

New Source Performance Standards (NSPS). The proposed modifications do not trigger NSPS applicability under 40 CFR Part 60, Subpart Da. NSPS pollutants for this facility are NOx,  $SO_2$ and PM10. A modification is defined for NSPS purposes to include any change in operation of a source that increases the maximum hourly emissions of a Part 60 regulated pollutant above the maximum achievable rate during the previous five years. CFR 60.14(h).

Prevention of Significant Deterioration. Planned upgrades to pollution control equipment as part of this proposed modification will result in net emissions decrease for certain criteria pollutants as a result of the project. Other pollutants may have increases below PSD significant levels. Accordingly, this modification will not require a major modification review. IPSC is providing to the DAQ supporting calculations and operating data.

Should you require any additional information, please contact Mr. Dennis Killian, Superintendent of Technical Services, at (435) 864-4414, or dennis-k@ipsc.com.

In as much as this notice of intent also constitutes a request for revision of IPSC's Title V Operating Permit, I hereby certify that, based on information and belief formed after reasonable inquiry, the statements and information in this document and the accompanying attachments are true, accurate, and complete.

I Gale Chapman

S. Gale Chapman

President, Chief Operations Officer, and Title V Responsible

Attachments:

Excel Spreadsheets (Emissions) Time Line Project Gantt Chart IPSC Check, \$1,200.00 NOI Fee

cc: Blaine Ipson, IPSC Jerry Hintze, IPSC Bruce Moore, LADWP CES Mike Nosanov, LADWP

Tim Conkin, LADWP CES John Schumann, LADWP Krishna Nand, Parsons Engineering James Holtkamp, LLG&M

Lynn Banks, IPSC

James Nelson, IPSC

Reed Searle, IPA

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NOI / PSD Calculations								
Operating & Production							-	
Parameter	Average Value   UoM		Post-Change Value					
Rated Output	875 Mwhe	he	950					
Fuel Use (Coal)	5,264,292 tons/y	s/yr	5,578,473					
Plant Operating Time	16,386 Unit h	hours	16,386					
Heat Value	11,872 BTU/I	J/lb	11,872					
Heat Input (Actual)	7,628 MMBtu/hr	Btu/hr	8,083					
Heat Input (Design)	8,352 MM	Btu/hr	9,225					
Heat Rate	9,564 Btu/K	/KWhr	9,475					
Flow - Stack	125,000,000 scfh	_	133,000,000					
Emissions					PSD Significance	PSD Major	Difference	PSD
Parameter/Pollutant	2 Yr Average Value   UoM		Post-Change Value	Change±/-	Levels	Trigger Value	(Trigger - Post)	Triggered?
PSD								
SO2	3586.31 Tons	St	3513.10	-73.21	40	3626.31	-113.21	z
SO2 % Removal	93.62 %		93.88					
NOx	25143.97 Tons	SL	24346.10	797.87	40	25183.97	-837.87	z
00	1317.06 Tons	St	1394.60	77.54	100	1417.06	-22.46	z
PM10	273.77 Tons	SL	283.51	9.75	15	288.77	-5.25	Z
Lead	0.087 Tons	St	0.123	980'0	009'0	0.687		Z
VOC	12.65 Tons	SL	13.40	0.75	40	52.65	-39.25	z
Beryllium	0.0102 Tons	SC	0.0014	-0.0088	0.0004	0.0106		z
Mercury	0.081 Tons	SL	0.105	0.024	0.100	0.181	920.0-	z
Fluorides (HF)	9.70 Tons	SL	10.16	0.46	က		-2.54	z
Sulfuric Acid	4.06 Tons	SI	4.05		7	11.06		z

PSD / NSPS Observations									ATTACHMENT 1: Worksheet	1: Worksheet B
Winderson Chemical Allocation	SO2 (loos)	SO2 % Removal	Nox (tons) CO (tons)	ns) PM10 (tons)	Lead (lbs)	XQC (lbs)	Beryllium (lbs)	Mercury (lbs)	Fluorides (HF	Sulfuric Acid, (Ibs.)
1000	3750	92.28	9688	90			3.57	270		
1007	50.15	92.05	22675				4.17	323		
1990	4781	92 67	25708				2 23	331		
0001	1608	93 57	24179			25394		123		
2000	3474	79.69	26109	1322 299		25204	1.89	201		
5 Year Avn	4058	92.8	23672	1265	1 200	25299		250	20854	8230
Cod av Class 1	3586	19 66	25144			25299				
TOLOGO Average + Cio lect	3636		25184	1417 289		105299	2.83	362		
Projected Actuals	3513	93 88	24346		4 245	26809	2.76	211		
									Maximum NOx	MaxImum SO2
The state of the s		Plant Operation	Bluilb	LB/MMBtu	Ibs/hr	LB/MMBtu	lbs/hr		Emission Rate	Emission Rate
ASSESSMENT OF THE PROPERTY OF	Coal Usage (Ions)		Coal HV	Ave Heat Input NOx Emission rate NOx Emission Rate SO2 Emission Rate	te NOx Emission Rate	SO2 Emission Bate	SO2 Emission Rate		(Last 5 years)	(Last 5 years)
1006	4310562		11860	6657 0.3	2564	200	489		6045	
1001	5158867	16564	11789	7343 0	2738	0.08	613		4875	
1998	5278344	16683	11823	7481 0 4	1 3082	0.07	513		5331	1279
1999	5244793	16462	11858	7556 0.3	2938	0.00	449		2002	
2000	5283790	16309	11885	7701 0 4	3202	0.06	426		544	
5 Year Avo	5055271	16275	11843	7348 0.	19 2905	0 0 0	498	498 MaxPrev. 5 yrs.	6045	1456
Last 2 Year Avo	5264292	16386	11872	7628 0	3070	0 00	438	438 Proposed Average		
Projected Actuals:	5578473	16386	11843	8064 0	2972	0.05	429	429 Proposed Max:	4613	
OPERATING CHANGES	Actual	Design								
	Max Heat Input	Max Heat Input (MIN	Btu/hr) Fuel Use (coal, tons) Heat	Hoat Rate Mibs/hr Steam	Mwhe	Siac				
Present Operation			- !		6.1	125,000,000				
	cada				6.9					_

ASSUMPTIONS.

All increases ( detreases based on coal use only. Fuel oil & other bulk chemical chemical use not expected to change. Estimated 15% contrial reduction with new NOx controls over oid.

Estimated 15% cominal reduction with new NOx controls over oid.

Estimated 15% cominal reduction with new NOx controls over oid.

Estimated 15% cominal reduction with new NOx controls over oid.

Projected of the new NOX calculated from NAPs ist.

Projected nominal efficiency improvement: 8 0%

Projected nominal edgeldy improvement: 8 6%

Projected ordinate appaidy improvement: 8 6%

Projected ordinate appaidy improvement: 8 6%

Projected uncontrolled NOX increase: 5 9%.

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ACGIH CI	Chronic A1 A1 A1 A1 Chronic Chronic Chronic Chronic Chronic Chronic Chronic Chronic	6.08 Acute 6.08 Acute 6.08 Acute 8.11 Chronic 6.58 Chronic 5.58 Chronic 54.2 Chronic	5.2.8 Chronic 6.14 Chronic 7.59 Chronic 2.56 Chronic 2.8.3 Chronic 28.3 Chronic 0.19 Chronic 26.1 Chronic	6. 16 Chronic 4.52 Chronic 8.98 Chronic 7. 88 Chronic 10.03 Acute A2 6. 18 Chronic 8.21 Acute	4. 45 Chronic 22.1 Chronic 21.1	16 Chronic 16 Chronic 09 Chronic		
Emissions (Ibs/yr) MW	39.70 286.75 814.20 814.20 814.20 814.20 86.20 86.20 347.20 347.20 347.20 30.284 30.284 32.13.20 43.32 53.32	2.85 1.385 3.179.73 44. 1.81.771 1.1771 5.03.33 78. 0.446 0.51 0.51 0.51 9.48 126.	1 4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	254.38 106 224.30 689 222.14 984 222.14 984 222.18 987 3.96 5.08 397.37 86 0.325.51 138.		의의에	96.408.29 20.313.45 8.108.13	
Listion	Fibs 10-12 Blu) Thruputitons) 2000jpstan*HV(Blu/lb))/10-12 Fibs 10-12 Blu) Thruputitons) 2000jpstan*HV(Blu/lb))/10-12 Fibs 10-12 Blu) Thruputitons) 2000jpstan*HV(Blu/lb))/10-12 Fibs 10-12 Blu) Thruputitons) 2000jpstan*HV(Blu/lb)/10-12 Fibs 10-12 Blu) Thruputitons) 2000jpstan*HV(Blu/lb)/HV(Blu/lb)	(Baton) Thruputitors)	(Baston) Thruputtions) ((Baston) Thruputtions)	(Baston) Thruputtions) ((Baston) Thruputtions)	(ibsten) Thruputions)	E=EF(lbs.ton) *Thrupud(lons) E=EF(lbs.ton) *Thrupud(lons) E=EF(lbs.ton) *Thrupud(lons) E=EF(lbs.ton) *Thrupud(lons) *Thrupud(lons) *Z000lbs.ton**	E=Concipon) Thruput(Mtons)*Control Efficiency(CE)*2000bs/ton E=Concipon)*Thruput(Mtons)*Control Efficiency(CE)*2000bs/ton E=Eff(bs/ton)*Thruput(tons)*Conc(%)*100*Control Efficiency(CE)	
(EF)	0.300 E=IEF 2.157 E=IEF 0.147 E=IEF 0.475	5.10E-07 [EEE] 2.50E-04 [EEE] 5.70E-04 [EEE] 1.50E-05 [EEE] 2.00E-04 [EEE] 3.80E+00 [EEE] 8.00E-04 [EEE] 1.10E-07 [EEE] 1.10E-07 [EEE] 2.70E-04 [EEE] 1.70E-04 [EEE] 1.70E-04 [EEE] 1.70E-04 [EEE] 1.70E-04 [EEE] 1.70E-04 [EEE]	7.30E-05   E-EE   3.90E-05   E-EE   1.30E-05   E-EE   1.20E-05   E	9.40E-05 E=E1 4.00E-05 E=E1 1.00E-06 E=E1 7.10E-07 E=E1 9.10E-07 E=E1 8.00E+00 E=E 6.70E-05 E=E1 6.70E-06 E=E1 6.70E-06 E=E1 5.80E-04 E=E1	1.00E-04 [E=E] 2.00E-04 [E=E] 2.00E-04 [E=E] 3.90E-04 [E=E] 1.70E-04 [E=E] 2.00E-05 [E=E] 2.50E-05 [E=E] 2.70E-05 [E=E] 2.70E-05 [E=E] 3.90E-04 [E=E] 4.30E-05 [E=E] 1.40E-05 [E=E] 4.30E-05 [E=E] 4.30E-05 [E=E] 7.00E-05 [E=E]	2.50E-05 E-E 3.70E-05 E-E 7.60E-08 E-E 2.00E-08 E-E	E=0 0 0645988 E=E	
Method Used* Factor (EF)	211-15 214-15 Calc(1) Calc(1) Calc(1) Calc(2) Calc(2) Calc(3) Calc(3) Calc(3) Calc(3) Calc(3) Calc(3) Calc(3) Calc(4) Calc(4) Calc(4) Calc(5) Calc(5) Calc(6)	211-12 211-13 211-13 211-13 211-13 211-13 211-12 211-12 211-12 211-13	211-13 211-13 211-13 211-13 211-13 211-13 211-13 211-13	211-13 211-13 211-13 211-12 211-12 211-12 Calc.(3) 211-13 211-13	2 11-13 2 11-13 2 11-13 2 11-13 2 11-13 2 11-12 2 11-13 2 11-13	2 1.1-13 2 1.1-13 2 1.1-13 Calc.(3)	Calc. (3)	AE SEC
(% emission of fuel conc.) Metho	AP421.  AP421.  AP421.  AP421.  AP421.  AP421.  AP421.  AP421.  AP421.  12% Eng Cal.  12% Eng Cal.  Eng Cal.  AP421.	AP42 AP42 AP42 AP42 AP42 AP42 AP42 AP42	AP42 AP42 AP42 AP42 AP42 AP42 AP42 AP42	AP42 AP42 AP42 AP42 AP42 AP42 AP42 AP42	AP4 AP4 AP4 AP4 AP4 AP4 AP4 AP4 AP4 AP4	AP4 AP4 AP4 Eng.	3% Eng. 3% Eng. 3% Eng. 3% Eng. 450%	ant operating hours = 16.386 bnc Filter Efficiency = 0.0047 bs/MMR
Factor (ibs/10^12 Btu) (%	0.92°(CA*PM)*0.63 3.1°(CA*PM)*0.85 1.2°(CA*PM)*1.1 3.3°(CA*PM)*0.5 3.7°(CA*PM)*0.5 1.7°(CA*PM)*0.5 3.4°(CA*PM)*0.69 3.4°(CA*PM)*0.69 3.4°(CA*PM)*0.60 3.8°(CA*PM)*0.60 4.4°(CA*PM)*0.60	0.0000051 (Ibarben) 2.5E-07 (Ibarben) 0.00057 (Ibarben) 0.00057 (Ibarben) 0.000015 (Ibarben) 0.0000015 (Ibarben) 3.8 (Ibarloh) 0.0018 (Ibarben) 1.1E-07 (Ibarben) 1.1E-07 (Ibarben) 0.0018 (Ibarben) 1.1E-07 (Ibarben) 0.001001	0.000073 (Isatem) 0.000038 (Isatem) 0.000038 (Isatem) 0.00003 (Isatem) 0.000002 (Isatem) 0.000003 (Isatem) 0.0000001 (Isatem) 0.0000001 (Isatem) 0.0000001 (Isatem) 0.00000038 (Isatem) 0.00000038 (Isatem)	0.00004 (Jeston) 0.00042 (Baston) 0.00044 (Baston) 0.0000012 (Baston) 0.0000011 (Baston) 0.0000011 (Baston) 0.0000012 (Baston) 0.0000012 (Baston) 0.000007 (Baston) 0.000007 (Baston) 0.0000007 (Baston) 0.0000001 (Baston) 0.000001 (Baston)	0.00016 (Bathon) 0.00053 (Bathon) 0.00053 (Bathon) 0.00053 (Bathon) 0.00017 (Bathon) 0.000023 (Bathon) 0.000023 (Bathon) 0.000023 (Bathon) 0.000023 (Bathon) 0.000027 (Bathon) 0.0000031 (Bathon) 0.0000031 (Bathon) 0.0000031 (Bathon) 0.0000031 (Bathon) 0.0000033 (Bathon)	0.000025 (hearton) 0.000037 (hearton) 0.000076 (hearton) 0.000002 (hear10+12 BTU)	0.0646 (lbs/ton)	410-4. Fait Soundaines > 100m)
(bpm) F	3.1 12 1.13 0.08 0.08 2.9 2.9 7.1 8.9 9.5 6.06 7.4 7.7 7.4						299 63 0.50%	15a R307.410-4 15 07.410-4. Boun M) X [ETF] )
POLLUTANT		Aconaphthere Aconaphthere Aconaphthere Aconaphthere Acotopherone Acotopherone Acotopherone Bartanege Berzolejanthracere Berzolejahrhracere	invitrence	statistical de la constanta del constanta de la constanta de l	Machine Bonder B	1,1,17,17,000,000,000,000,000,000,000,00	Hydrogen Chlonde Hydrogen Fluoride Sulfunc Acid Sulfunc Acid (1) By ash fraction derivative (2) By stack test (2) By stack test (3) By stack test (3) By stack test	(4) By SoCo's Paper (4) By SoCo's Paper (4) By SoCo's Paper (5) Realized HAP emission increases calcutated per Utan R307-410-4, (7) Convent point to mann3: T.U/(point) X MV / 24.45 (2) E impact (acutat/chonic/carcinogenic) (ETF = Emission Threshold Factor (Table IV-2, R307-410-4, Bounds (TLY = Threshold Link Tables (ACGIN 2001 version) (ETF = Emission Threshold Value (Tuhn) = (TLV) X (ETF)) (1SL = Toxic Screening Level (Tul/2)

HP TURBINE DEN						TACHMEN		Γ
99-00 Average lbs/mmbt	U							L
			ļ <u>.</u>				<del> </del>	↓-
inlet	stack	% reduction		114410 000 00			<del></del>	╁
0.7744		93.6209 93.8760		U1/U2 '99-00 average 4% reduction stack lbs/m	<u></u>		<del> </del>	╁
0.7744 0.7744				97 3657% reduction (4%)		hher efficienc	.v)	H
0.7744	0.0204	31.3031	<del> </del>	37 3037 to reduction (4 M	micrease in scre	Doer emercine	7	t
	<del> </del>	<del> </del>	<del> </del>					T
1999			<del> </del>		†			Γ
Unit One				Unit Two				Г
0.111.0.110								
Coal Burned (tons)	2,472,213			Coal Burned (tons)	2,772,580			L
Heating Value btu/lb	11,858			Heating Value btu/lb	11,858			L
inlet SO2 lbs/mmbtu	0.7963			Inlet SO2 lbs/mmbtu	0.7867			L
Stack SO2 lbs/mmbtu	0.0479			Stack SO2 lbs/mmbtu	0.0538			⊢
Inlet Tons SO2	23,343.93	100000000000000000000000000000000000000	I com my codera.	Inlet Tons SO2	25,864.54	And the little states		┢
Stack Tons SO2			(EUR)	Stack Tons SO2	93.1613		CUCA	⊢
% Removal (lbs/mmbtu)	93.9847 93.9847	<del> </del>		% Removal (lbs/mmbtu) % Removal (tons)	93.1613	<del> </del>	1	⊢
% Removal (tons) % Removal (EDR tons)	93.9847	0.69	<b>——</b>	% Removal (tons)	91.7578	1.40	<del>                                     </del>	H
76 Removal (EDR tons)	33.2039	0.09	<del>                                     </del>	w removal (EDR IONS)	31.7376	1.70		1
2000		<del> </del>			-	<del> </del>		Г
Unit One		<del> </del>		Unit Two	<del>                                     </del>			Ι.
		<u> </u>						Γ
Coal Burned (tons)	2.799,081			Coal Burned (tons)	2.484,709			L
Heating Value btu/lb	11,885			Heating Value btu/lb	11,885			Ľ
Inlet SO2 lbs/mmbtu	0.7712			Inlet SO2 lbs/mmbtu	0.7432		<b></b>	L
Stack SO2 lbs/mmbtu	0.0482			Stack SO2 lbs/mmbtu	0.0477		<b>  </b>	$\vdash$
Inlet Tons SO2	25,655.57			Inlet Tons SO2	21,947.27			L
Stack Tons SO2		海河 855.40	(EDR)海绵	Stack Tons SO2			(EUS)	H
% Removal (lbs/mmbtu)	93.7500			% Removal (ibs/mmbtu)	93.5818	<b> </b>	<del> </del>	⊢
% Removal (tons)	93.7500	0.60		% Removal (tons)	93.5818 92.6223	. 0.96		⊢
% Removal (EDR tons)	92.7692	0.98		% Removal (EDR tons)	92.0223	. 0.90	<del></del>	-
1000 0000 4		ntina Station	<u> </u>				<del>                                     </del>	Н
1999-2000 Average Inte	mountain Genera	ating Station	<u> </u>		<del> </del>		1	<u> </u>
% Removal (lbs/mmbtu)	93.6194	<del>                                     </del>		Inlet lbs/mmbtu	-034507793		1	_
% Removal (tons)	93.6194			Stack lbs/mmbtu	0.0494		1	┌
% Removal (EDR tons)	92.6098			Old Old Tool Tool Tool Tool Tool Tool Tool To				Г
70 Tromovar (CDTC tone)		·				-		
		-						L
Dense Pack - Intermot	Intain Generating	Station						L
PREMODIFICATION	1999 - 2000 Avera		d)	POST MODIFICATION (		odification)		<u> </u>
Coal Burned (tons)	5,268,249			Coal Burned (tons)	5.578,473			<u> </u>
Heating Value btu/lb	11,871			Heating Value btu/lb	11,871		<b>├</b>	$\vdash$
Inlet SO2 lbs/mmbtu	0.7744			Inlet SO2 lbs/mmbtu Stack SO2 lbs/mmbtu	0.7744		<del>  </del>	_
Stack SO2 lbs/mmbtu	0.0494 48,430.50	54,170.45		Inlet Tons SO2	51,282.36	57403 69	Actual Proje	-
Inlet Tons SO2 Stack Tons SO2		35.3586.25		Stack Tons SO2	3 271 37	379747	(FDR Proje	ect
% Removal (lbs/mmbtu)	93.6209			% Removal (lbs/mmbtu)	93.6209	93.68		
19 Kelilovai (losifilitolo)	33.0203	33.30		70 (Certio Val (Ioo) (III) (Ioo)	50.0250			Г
								Ξ
				POST MODIFICATION (	W/Scrubber Mod	lification)		Ĺ
	Tons of SO2 Red	luction		4% reduction stack lbs/m	mbtu			
	130.85			Coal Burned (tons)	5,578,473		ļ	_
	*# <b>373</b> 7375	(EDR Projec	ted)	Heating Value btu/lb	11,871		<b>├</b>	_
				Inlet SO2 lbs/mmbtu	0.774		<b>├</b>	-
		<u></u>		Stack SO2 Ibs/mmbtu	0.047424	57402.00	Actual Proje	
				Inlet Tons SO2 Stack Tons SO2	51,282.36	57403.69 33,513.10	/FDR Proje	المات
		<del> </del>		% Removal (lbs/mmbtu)	93.8760	93.88		
				70 INEMIOVAL (IUS/IIIIIU(U)	33.0700	35.00		
					<del> </del>		<del>                                     </del>	_
								_
				POST MODIFICATION (V	N/Scrubber Mod	lification)		
	Tons of SO2 Red	uction		97.3657% reduction (4%			y)	
	1,920.44			Coal Burned (tons)	5,578.473			_
	2074.06	(EDR Projec	ted)	Heating Value btu/lb	11,871			
(				Inlet SO2 lbs/mmbtu	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		<u> </u>	_
				Stack SO2 lbs/mmbtu	0.0204		$\Box$	_
	!	1		Inlet Tons SO2	51,282.36		Actual Proje	
				C11, T CO2	1.350.93	<b>多利 512 19</b>	(EDR Project	cte
				Stack Tons SO2				
				% Removal (lbs/mmbtu)	97.3657		<b> </b>	
								<u>-</u>
				% Removal (lbs/mmblu)	97.3657	Charles		
Stack SO2 tons calculate	d from lbs/mmbtu a	are less than		% Removal (lbs/mmblu)	97.3657	Stack flow.		  

## ATTACHMENT 1: Worksheet E

#### **CO Calculations**

Dense Pack - Interme	ountain Generating Station		
PREMODIFICATION	1999 - 2000 Average	POST MODIFICATIO	N
Coal Burned (tons)	5,268,249	Coal Burned (tons)	5,578,473
CO E.F. (lb/ton)	0.50	CO E.F. (lb/ton)	0.50
CO Emissons (tons)	1317.06	CO Emissons (tons)	1394.62

Tons of CO increase 77.56

AP-42 Table 1.1-3

#### **ATTACHMENT 1**: Worksheet F

#### DENSE PACK PM10 COAL USAGE CALCULATION SUMMARY

#### YEARLY INVENTORY

5,578,473	Tons coal received Railcar Unloading
5,578,473	Tons of coal fed to both Units
2,789,237	Tons of coal fed to Unit 1
2,789,237	Tons of coal fed to Unit 2
11,800	Coal heating value (Btu/lb)
25.1	Coal pile (acres)
0.0056	Unit 1 Particulate lbs/mmbtu (tsp)
0.0036	Unit 2 Particulate lbs/mmbtu (tsp)

## UNIT 1 FABRIC FILTER PARTICULATE EMISSION (online)

169.5677 TPY Particulate PM10

AP 42 Table 1.1-6

## UNIT 2 FABRIC FILTER PARTICULATE EMISSION (online)

109.0078 TPY Particulate PM10

AP 42 Table 1.1-6

## COAL TRAIN UNLOADING DUST COLLECTORS A,B,C,D

0.0625 TPY Particulate PM10

#### COAL TRUCK UNLOADING DUST COLLECTOR

0.0000 TPY Particulate PM10

Included in train unloading

#### COAL RESERVE RECLAIM DUST COLLECTOR

0.0020 TPY Particulate PM10

10% of Coal Crusher Emissions

#### COAL SAMPLE PREPARATION DUST COLLECTOR

0.0000 TPY Particulate PM10

### COAL TRANSFER BUILDING #1 DUST COLLECTOR

0.0156 TPY Particulate PM10

## COAL TRANSFER BUILDING #2 DUST COLLECTOR

0.0312 TPY Particulate PM10

## COAL TRANSFER BUILDING #4 DUST COLLECTOR

0.0195 TPY Particulate PM10

#### COAL CRUSHER BUILDING DUST COLLECTOR

0.0195 TPY Particulate PM10

#### **ACTIVE COAL STACKOUT (fugitive)**

3.9049 TPY Particulate PM10

#### DUST COLLECTOR 13A & 13B

0.0312 TPY Particulate PM10

#### **DUST COLLECTOR 14A & 14B**

0.0156 TPY Particulate PM10

#### **COAL PILE FUGITIVE EMISSIONS**

0.8368 TPY Particulate PM10

#### 283.5145 TPY PM10 (COAL ONLY)

EF found in AP-42 Table 11.19.2-1 site dust collectors for coal, limestone, lime vacuum sys. and soda ash PM10 and PM2.5. Using same ratio of PM10 to PM2.5 found with emissions at stack.

Use cumulative Mass % <= Stated Size in AP-42 Table 1.1-5 for percentages of PM10 and PM2.5 as a ratio of TSP.

PM10 = 92% of TSP

PM2.5 = 53% of TSP

3 2004	4/1/2004		CE 1541 - 1574 - 1544 -					33		4/1/2004	03			MARKET CONTROL 4/1/2004	######################################	4/1/2004	4/2/2003	23			.СН 			2	03	03	03	03		03	003
2000 2001 2003	1/2/2001	1/15/2001 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1	2/1/2001	4/2/2001 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	4/2/2001 . B. Dental Control of the	4/2/2001 - ACTIVE OF THE CONTRACTOR AND	4/2/2001 (* 3/2/2014   1/2/2014	1/2/2001 C.	3/1/2001 ( * 18.5 ) Production of the state	4/2/2001	5/2/2001 (Company of the Company of	4/2/2001 [17.200] 4/1/2002	4/2/2001 Sure 1000 100 Sure 1000 Sur	4/2/2001	1/2/2002	1/2/2002	1/2/2001	1/15/2001	2/1/2001	3/1/2001	1/2/2002	1/2/2002 - 1 - 4 - 4 - 4 - 4 - 4 - 4 - 4 - 4 - 4	1/2/2002	1/2/2001	1/2/2002 1/2/2003 1/2/2000 1/2	3/1/2001	5,1/2001 Land Comment of the Comment	1/2/2002 CONTROLLE AND THE PROPERTY OF THE PRO	4/2/2001	4/2/2001 Signment on Apparation on the Apparation of the Apparatio	1/2/2002 (55)35-2003 (55)35-2003
Task Name	Unit 2 Projects	HP Turbine Retrofit	Cooling Tower Performance Upgrade	Boiler Safety Valve Addition	Generator Cooling Enhancements	Isophase Cooling Enhancements	Large Motor Bus Loading Equalization	Boiler Feed Pump Performance Upgrade	Main Step-up Transformer Cooling	NOx Reduction Project	Scrubber Wall Ring	Generator SCW O2 Monitoring	HP Heater Drain Line Mods	Boiler Modifications	Cooling Tower Makeup Modifications	Cooling Tower Electrical Redundancy	Unit 1 Projects	HP Turbine Retrofit	Cooling Tower Performance Upgrade	Boiler Safety Valve Addition	Generator Cooling Enhancements	Isophase Cooling Enhancements	Large Motor Bus Loading Equalization	Boiler Feed Pump Performance Upgrade	Main Step-up Transformer Cooling	NOx Reduction Project	Scrubber Wall Ring	Generator SCW O2 Monitoring	HP Heater Drain Line Mods	Boiler Modifications	Cooling Tower Electrical Redundancy

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